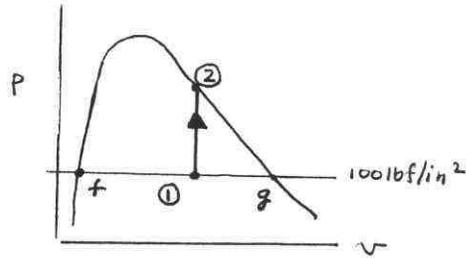
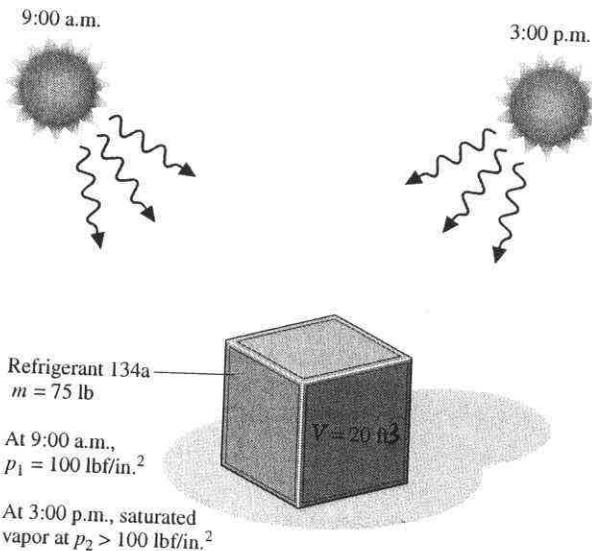


PROBLEM 3.59

KNOWN: Data are provided for Refrigeration 134a in a closed, rigid tank exposed to solar radiation.

FIND: For the process of the refrigerant, determine the initial temperature, final pressure, and  $Q$ .

SCHEMATIC & GIVEN DATA:



ENGR. MODEL

1. The R134a in the tank is the closed system.
2. For the system,  $W = 0$ .
3. Kinetic and potential energy effects play no role.

Fig. P3.59

ANALYSIS: At the initial state,  $v_1 = \frac{V}{m} = \frac{20 \text{ ft}^3}{75 \text{ lb}} = 0.2667 \frac{\text{ft}^3}{\text{lb}}$ . Since  $v_f < v_1 < v_g$ , the initial state is in the two-phase, liquid-vapor region. Further, since mass and volume are each constant, there is no change in specific volume for the process:  $v_2 = v_1$ .

(a) Since the initial state is a two-phase, liquid-vapor mixture at  $100 \text{ lbf/in}^2$ , the initial temperature is the corresponding saturation temperature. From Table A-11E,  $T_1 = 79.17^\circ\text{F}$ .

(b) Interpolating in Table A-11E with  $v_2 = v_g = 0.2667 \text{ ft}^3/\text{lb}$ , we get  $p_2 = 174.4 \text{ lbf/in}^2$  and  $u_2 = 107.93 \text{ Btu/lb}$ .

(c) Reducing an energy balance  $\Delta U + \Delta KE + \Delta PE = Q_{12} - W_{12}$ , we get

$$Q_{12} = m(u_2 - u_1)$$

Finding  $u_1$  requires the quality at state 1. That is, with  $v_f$  and  $v_g$  from Table A-11E at  $100 \text{ lbf/in}^2$ ,

$$x_1 = \frac{v_1 - v_f}{v_g - v_f} = \frac{0.2667 - 0.01332}{0.4747 - 0.01332} = 0.549$$

Then,  $u_1 = u_f + x_1(u_g - u_f) = 36.75 + (0.549)(103.68 - 36.75) = 73.49 \text{ Btu/lb}$

Finally,  $Q_{12} = 75 \text{ lb}(107.93 - 73.49) \frac{\text{Btu}}{\text{lb}} = 2583 \text{ Btu}$

